

Alternate Hydraulic Fracturing Fluids

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Introduction

- Overview of the project
- Calculations of flow rates of alternate fluids
- Thermal Effects
- Economics



Overview of Project

- For the spring semester our team is comparing our findings from the fall semester from the data provided by “Triangle Petroleum Corporation,” and use this data to determine the possible application of alternative hydraulic fracturing methods.
- Our team is using data for two wells located in McKenzie County, ND.
- We will compare the feasible methods to the traditional method and determine the best economic choice for our wells.



Premise

- Looking at liquid carbon dioxide, liquid nitrogen, and liquid natural gas
- In addition we are looking at energized fractures
- To compare the alternative fluids assuming the same fracture efficiencies
- Allow us to obtain flow rates and liquid volumes from the volume of the wings in the original fracture
- This is needed to complete economic analysis

Difficulties With the PKN Model

- Assumptions
- Water loss
- Efficiencies
- Thermal effects

Adaptation of PKN Model

- Last semester PKN assumptions
 - ν
 - G
 - μ

| Treatment 5 | | | |
|-------------|------------------|-------|-------|
| | $\mu, c_p = 200$ | | |
| ν | 0.2 | 0.3 | 0.4 |
| G, MPa | 1.992 | 1.743 | 1.494 |
| E, MPa | 3.188 | 2.440 | 1.792 |

PKN Analysis

| 70% Carbon Dioxide 30% Slick Water Flow Rates For Treatment 5 | | | | | | | | | | | |
|---|----------|-------------------|--|---------------------------------|----------|-------------------|--|---------------------------------|----------|-------------------|--|
| water viscosity, cp=200 | | | | | | | | | | | |
| Treatment 5 for Pois Ratio = .2 | | | | Treatment 5 for Pois Ratio = .3 | | | | Treatment 5 for Pois Ratio = .4 | | | |
| v= | 0.20 | | | v= | 0.30 | | | v= | 0.40 | | |
| G= | 1.99E+08 | Pa | | G= | 1.74E+08 | Pa | | G= | 1.49E+08 | Pa | |
| Wmax= | 0.02 | m | | Wmax= | 0.02 | m | | Wmax= | 0.02 | m | |
| L= | 99.36 | m | | L= | 99.36 | m | | L= | 99.36 | m | |
| μ = | 0.29 | Pa*s | | μ = | 0.29 | Pa*s | | μ = | 0.29 | Pa*s | |
| Q= | 0.05 | m ³ /s | | Q= | 0.05 | m ³ /s | | Q= | 0.05 | m ³ /s | |
| | 784.07 | gpm | | | 784.07 | gpm | | | 784.07 | gpm | |
| | 18.67 | bpm | | | 18.67 | bpm | | | 18.67 | bpm | |
| water viscosity, cp=470 | | | | | | | | | | | |
| Treatment 5 for Pois Ratio = .2 | | | | Treatment 5 for Pois Ratio = .3 | | | | Treatment 5 for Pois Ratio = .4 | | | |
| v= | 0.20 | | | v= | 0.30 | | | v= | 0.40 | | |
| G= | 4.68E+08 | Pa | | G= | 4.10E+08 | Pa | | G= | 3.51E+08 | Pa | |
| Wmax= | 0.02 | m | | Wmax= | 0.02 | m | | Wmax= | 0.02 | m | |
| L= | 99.36 | m | | L= | 99.36 | m | | L= | 99.36 | m | |
| μ = | 0.29 | Pa*s | | μ = | 0.29 | Pa*s | | μ = | 0.29 | Pa*s | |
| Q= | 0.12 | m ³ /s | | Q= | 0.12 | m ³ /s | | Q= | 0.12 | m ³ /s | |
| | 1842.89 | gpm | | | 1843.00 | gpm | | | 1842.62 | gpm | |
| | 43.88 | bpm | | | 43.88 | bpm | | | 43.87 | bpm | |



PKN Analysis

| 70% Nitrogen 30% Slick Water Flow Rates For Treatment 5 | | | | | | | | | | | |
|---|----------|-------------------|---------------------------------|---------|----------|---------------------------------|--|---------|----------|-------------------|--|
| water viscosity, cp=200 | | | | | | | | | | | |
| Treatment 5 for Pois Ratio = .2 | | | Treatment 5 for Pois Ratio = .3 | | | Treatment 5 for Pois Ratio = .4 | | | | | |
| v= | 0.20 | | | v= | 0.30 | | | v= | 0.40 | | |
| G= | 1.99E+08 | Pa | | G= | 1.74E+08 | Pa | | G= | 1.49E+08 | Pa | |
| Wmax= | 0.02 | m | | Wmax= | 0.02 | m | | Wmax= | 0.02 | m | |
| L= | 99.36 | m | | L= | 99.36 | m | | L= | 99.36 | m | |
| μ = | 0.16 | Pa*s | | μ = | 0.16 | Pa*s | | μ = | 0.16 | Pa*s | |
| Q= | 0.09 | m ³ /s | | Q= | 0.09 | m ³ /s | | Q= | 0.09 | m ³ /s | |
| | 1428.31 | gpm | | | 1428.31 | gpm | | | 1428.31 | gpm | |
| | 34.01 | bpm | | | 34.01 | bpm | | | 34.01 | bpm | |
| water viscosity, cp=470 | | | | | | | | | | | |
| Treatment 5 for Pois Ratio = .2 | | | Treatment 5 for Pois Ratio = .3 | | | Treatment 5 for Pois Ratio = .4 | | | | | |
| v= | 0.20 | | | v= | 0.30 | | | v= | 0.40 | | |
| G= | 4.68E+08 | Pa | | G= | 4.10E+08 | Pa | | G= | 3.51E+08 | Pa | |
| Wmax= | 0.02 | m | | Wmax= | 0.02 | m | | Wmax= | 0.02 | m | |
| L= | 99.36 | m | | L= | 99.36 | m | | L= | 99.36 | m | |
| μ = | 0.16 | Pa*s | | μ = | 0.16 | Pa*s | | μ = | 0.16 | Pa*s | |
| Q= | 0.21 | m ³ /s | | Q= | 0.21 | m ³ /s | | Q= | 0.21 | m ³ /s | |
| | 3357.11 | gpm | | | 3357.31 | gpm | | | 3356.63 | gpm | |
| | 79.94 | bpm | | | 79.94 | bpm | | | 79.92 | bpm | |



PKN Analysis

| Liquid Natural Gas Flow Rates For Treatment 5 | | | | | | | | | |
|---|----------|-------------------|---------------------------------|----------|-------------------|---------------------------------|----------|-------------------|--|
| water viscosity, cp=200 | | | | | | | | | |
| Treatment 5 for Pois Ratio = .2 | | | Treatment 5 for Pois Ratio = .3 | | | Treatment 5 for Pois Ratio = .4 | | | |
| v= | 0.20 | | v= | 0.30 | | v= | 0.40 | | |
| G= | 1.99E+08 | Pa | G= | 1.74E+08 | Pa | G= | 1.49E+08 | Pa | |
| Wmax= | 0.02 | m | Wmax= | 0.02 | m | Wmax= | 0.02 | m | |
| L= | 99.36 | m | L= | 99.36 | m | L= | 99.36 | m | |
| μ= | 0.00024 | Pa*s | μ= | 0.00024 | Pa*s | μ= | 0.00024 | Pa*s | |
| Q= | 59.89 | m ³ /s | Q= | 59.89 | m ³ /s | Q= | 59.89 | m ³ /s | |
| | 949305 | gpm | | 949305 | gpm | | 949305 | gpm | |
| | 22604 | bpm | | 22603 | bpm | | 22604 | bpm | |
| water viscosity, cp=470 | | | | | | | | | |
| Treatment 5 for Pois Ratio = .2 | | | Treatment 5 for Pois Ratio = .3 | | | Treatment 5 for Pois Ratio = .4 | | | |
| v= | 0.20 | | v= | 0.30 | | v= | 0.40 | | |
| G= | 4.68E+08 | Pa | G= | 4.10E+08 | Pa | G= | 3.51E+08 | Pa | |
| Wmax= | 0.02 | m | Wmax= | 0.02 | m | Wmax= | 0.02 | m | |
| L= | 99.36 | m | L= | 99.36 | m | L= | 99.36 | m | |
| μ= | 0.00024 | Pa*s | μ= | 0.00024 | Pa*s | μ= | 0.00024 | Pa*s | |
| Q= | 140.77 | m ³ /s | Q= | 140.78 | m ³ /s | Q= | 140.75 | m ³ /s | |
| | 2231249 | gpm | | 2231385 | gpm | | 2230931 | gpm | |
| | 53127 | bpm | | 53130 | bpm | | 53120 | bpm | |



Results of PKN Model

| Gardner Denver C-2500 pump at 20,000 psi pumping 191 GPM | | | | | | | | | |
|--|------------------------------------|-----|-----|------------------------------|-----|-----|--------------------|-------|-------|
| | 70% Carbon Dioxide 30% Slick Water | | | 70% Nitrogen 30% Slick Water | | | Liquid Natural Gas | | |
| Viscosity | 200 | 470 | 925 | 200 | 470 | 925 | 200 | 470 | 925 |
| # of pumps | 5 | 10 | 19 | 8 | 18 | 35 | 5000 | 11700 | 23000 |

Thermal Calculations

- Have been made based on a flow-back report from *Triangle Petroleum*.
- The flow-back report has water temperature leveling off at approximately 170 degrees Fahrenheit.
- By using the specific heat capacities of each fluid type, and comparing that to the temperature change of water, our team has estimated the bottom-hole temperature for each fluid type.
- Although this method is not exact, it is acceptable for this scenario as it uses real production data to estimate temperature.
- This method also has the benefit of giving specific data to apply to viscosity since liquid CO₂ changes with temperature.

Thermal Calculations

- Specific Heat by fluid type:
 - Water – 4480 J/kg*K
 - LNG – 3510.376 J/kg*K
 - Liquid Nit. – 2040 J/kg*K
 - Liquid CO₂ – 2272.72 J/kg*K
- Bottom-hole temperature estimates:
 - Water – 410.928 K
 - LNG – 189.141 K
 - Liquid Nit. – 211.555 K
 - Liquid CO₂ – 315.113 K

Thermal Stresses

- Thermal stress in the formation is calculated using the equation:

$$\sigma = E(1+\nu)\alpha\Delta T$$

- $\nu \sim$ Poisson's Ratio – 0.3 is an acceptable value for the Bakken
- $\alpha \sim$ Unit temperature change – We use $1 \times 10^{-5} \text{ K}^{-1}$
- $\Delta T \sim$ This value is calculated for each fluid type based on its specific heat, and the values we use are:

$$\text{CO}_2 \sim 95.82 \text{ K}$$

$$\text{N}_2 \sim 199.37 \text{ K}$$

$$\text{LNG} \sim 221.79 \text{ K}$$

- The final value used in the equation for thermal stresses is the Modulus of Elasticity.

Modulus of Elasticity

- Our team found discrepancies in the value to use for Modulus of Elasticity. Based on the PKN model, which assumes no water loss, our team calculated a value of 0.2441 GPa for this formation.
- These wells actually lose close to 90% of pumped water to the formation, and as a result the rock appears “softer” than it really is.
- Research has indicated that appropriate values for Modulus of Elasticity in the Bakken are between 5 – 65 GPa



Calculated Thermal Stresses

| | E = 0.2441 GPa | E = 5 GPa | E = 20 GPa | E = 40 GPa | E = 65 GPa |
|------------------------------|----------------|-----------|------------|------------|------------|
| σ_{CO_2} (psi) | 44.1 | 903.3 | 3613.4 | 7226.7 | 11,743.4 |
| σ_{N_2} (psi) | 91.76 | 1879.6 | 7518.2 | 15,036.4 | 24,434.2 |
| σ_{LNG} (psi) | 102.08 | 2091.4 | 8365.7 | 16,731.4 | 27,181.9 |

Selection Criteria

- Our formation opening stress is 13,396 psi
- This means that only N₂ and LNG are feasible for our wells.
- These fluids can be used to fracture the wells thermally for Modulus of Elasticity Values above 35.63 GPa for N₂ and 32.03 GPa for LNG.

Economics of Alternative Fracturing Treatment

- Information regarding service company day rates varies
- A contact from Oxbow Energy Services was kind enough to give us a rough estimate
- Most service companies package all fracturing treatment services into a day rate
- While they may vary, a current day rate is generally all inclusive (pump trucks, blenders, chemical pumpers, control van)
- Water disposal is the responsibility of the operator
- \$350M per day for 5 stage treatments is currently a good assessment for the industry

Economics of Alternative Fracturing Treatment

- \$350M for 5 stages is accurate (plus or minus depending on treatment)
- A 15% premium is a good figure for a CO₂/Nitrogen energized or gas/liquid fracturing treatment
- \$403M would be the high end for a day rate
- 3.4MM gallons of water needed for regular “slick water” treatment (this is for the entire fracturing job)
- 119M lbs of proppant per stage=1.8M tons for entire treatment
- Cheaper 40/70 sand used for initial breakdown pressure=\$70/ton (only 3100lbs used)
- Carbo-ceramic lightweight ISP 20/40 composes (total cost for all stages=\$123MM)
- Purchase freshwater from WAWSA at \$20/1000 gallons
- Total job requires purchase of \$68.8M in freshwater at industrial rates.
- \$0.12-\$0.25 per gallon to dispose of wastewater
- Assuming \$0.20, at 82M gallons, total cost per stage is \$16.4M
- Total wastewater costs for well at \$154M for entire treatment
- Total cost per well to perform slick water hydraulic treatment is \$2.5MM
- We are not re-injecting water, but this could be a possibility. Environmentally speaking we are going to retreat water based on statues for storage and disposal.



Economics of Alternative Fracturing Treatment

- N₂ cost at approximately \$0.10 per liquid gallon
- Assumption of 75% flowback performance
- With 70% N₂ hybrid treatment, \$24M
- 30% at same disposal/purchase costs gives us \$91M in treatment costs
- Service company upcharge for extra pumps and equipment is ascertained to be 20% higher
- Total charge for service is \$2.5MM
- Entire cost of hybrid fracturing treatment is \$2.75MM

Economics of Alternative Fracturing Treatment

- CO₂ costs are approximately \$40 per ton at wholesale rates
- Translates to \$0.18 per gallon
- Extrapolating these figures with a 70/30 hybrid fracturing treatment gives us a total well cost of \$2.77MM
- Figures include higher loss rate of CO₂ to formation due to miscibility

Conclusion

- Results of the PKN model
- LNG has best thermal stress
- Energized nitrogen most feasible alternative fluid
- Slick water most economical

Questions?