



bio**solve**

The logo features the word "biosolve" in a sans-serif font. The letters "bi" and "os" are rendered in a vibrant green color with a subtle gradient and are integrated with stylized plant motifs. The letter "b" has a stem and a leaf at the top. The letter "i" is a simple vertical bar with a stem and two leaves at the top. The letter "o" is a solid green circle with a stem and two leaves at the top. The letter "s" is black with a stem and two leaves at the bottom. The letters "olve" are solid black. The background consists of a blue sky with white clouds and a white ground line.

Created By: Alyssa Hughes

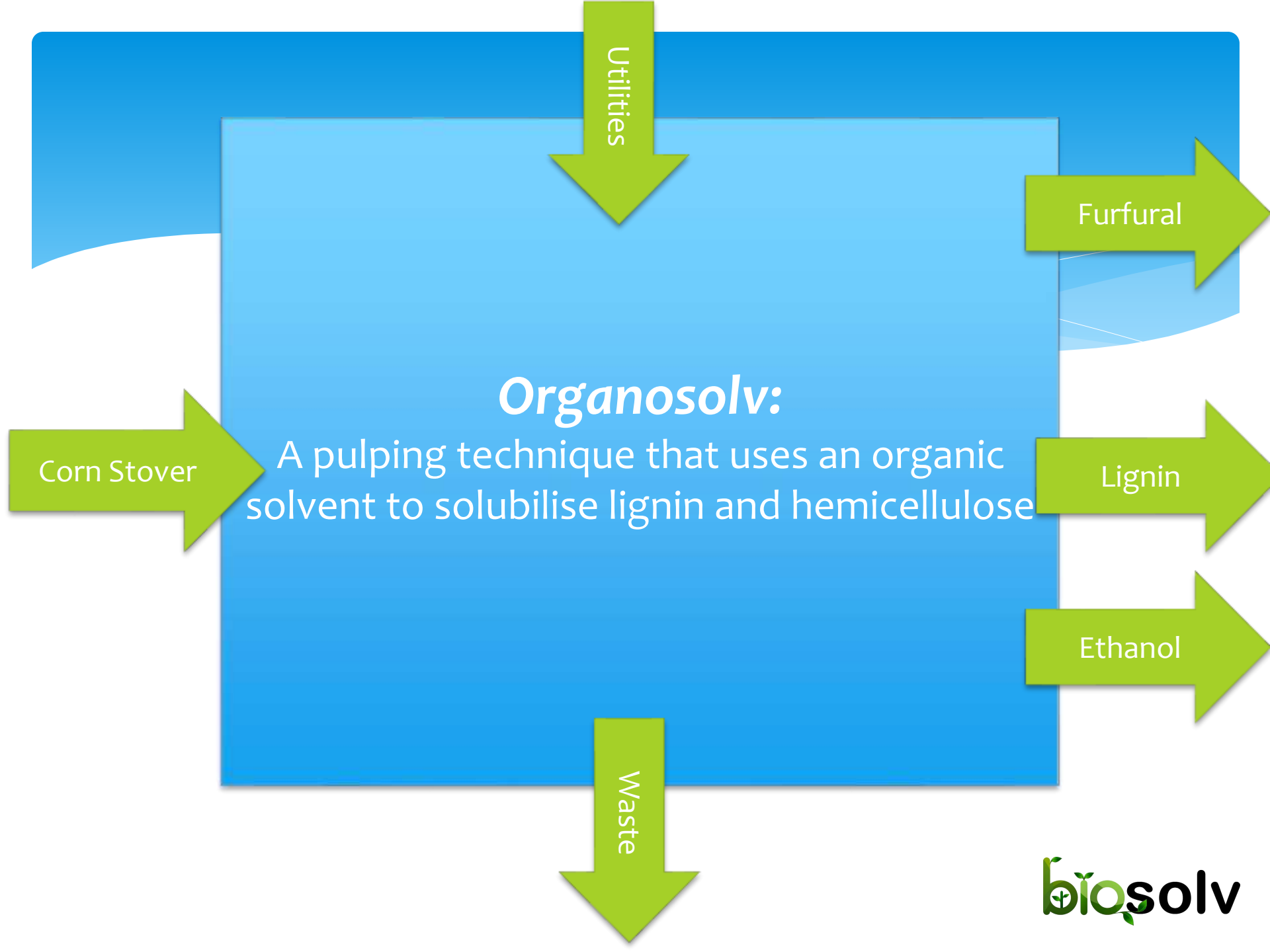
The Implementation of Organosolv Pretreatment

Team Members:

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Neuberger

Project Proposal

- * Our goal is to implement an Organosolv process into an existing cellulosic ethanol plant that can produce 20,000 lb/hr of fuel grade ethanol.



Organosolv:

A pulping technique that uses an organic solvent to solubilise lignin and hemicellulose

Corn Stover

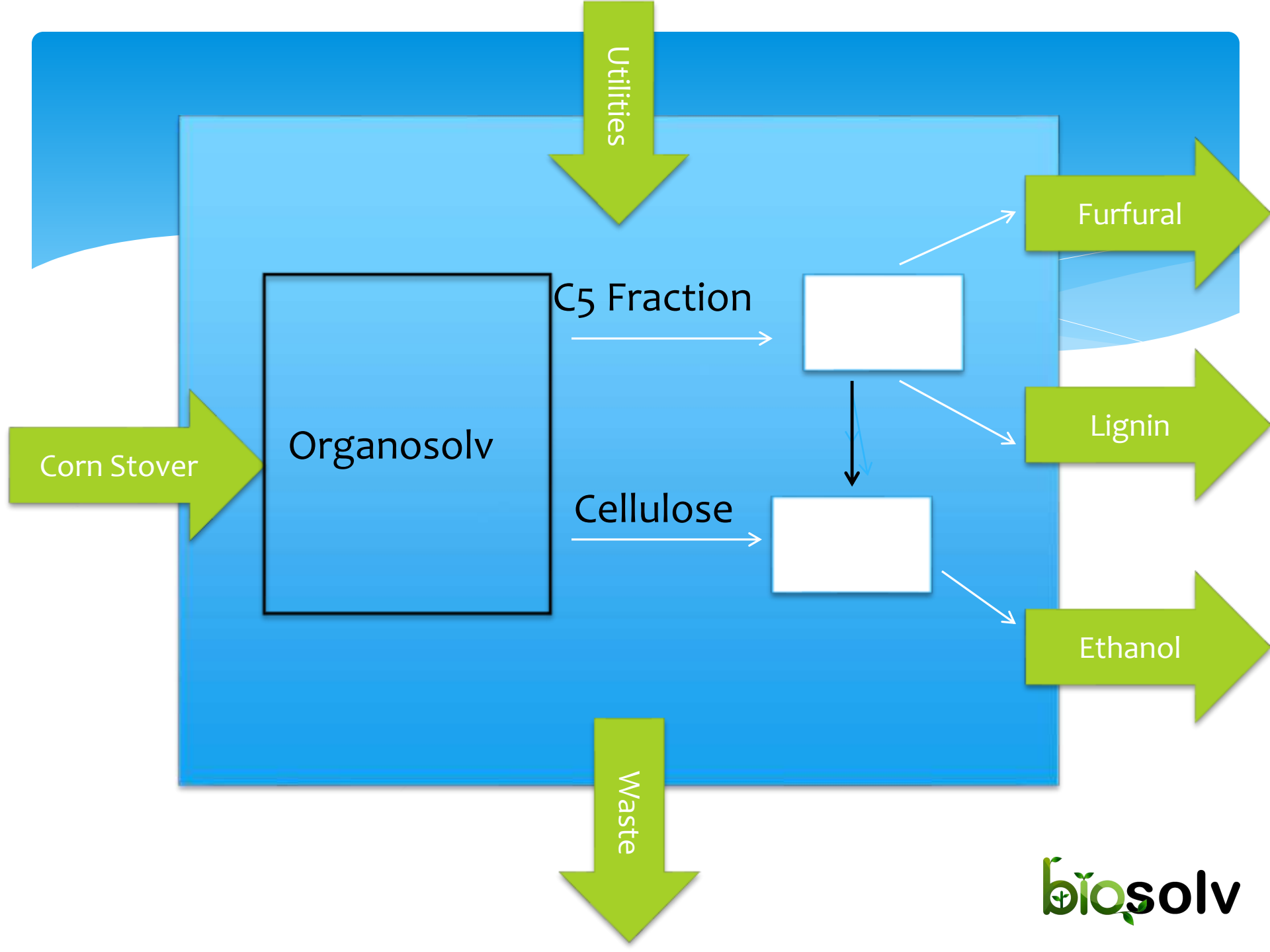
Utilities

Furfural

Lignin

Ethanol

Waste



Corn Stover

Organosolv

Utilities

C5 Fraction

Cellulose

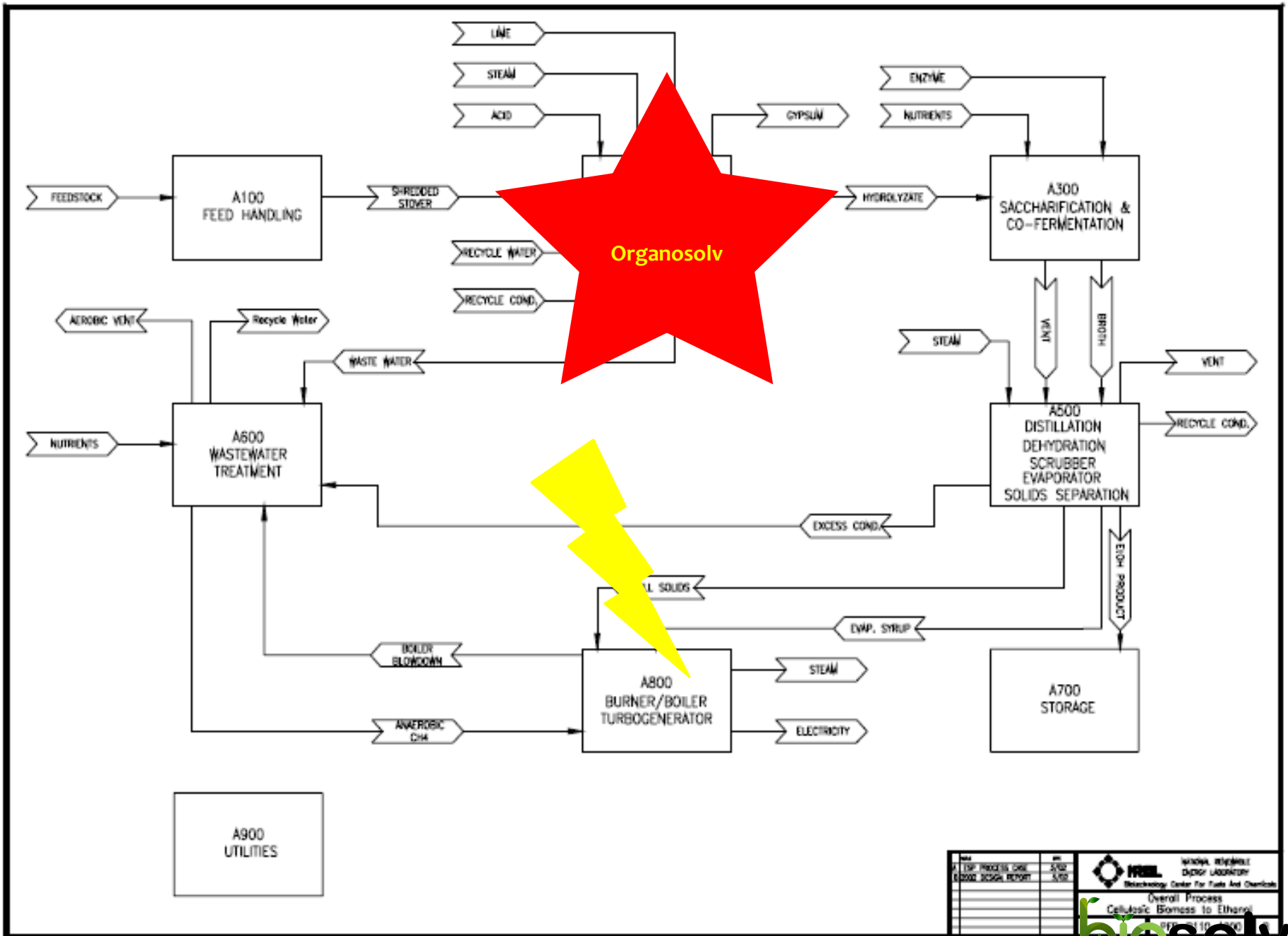
Furfural

Lignin

Ethanol

Waste

bio-solv



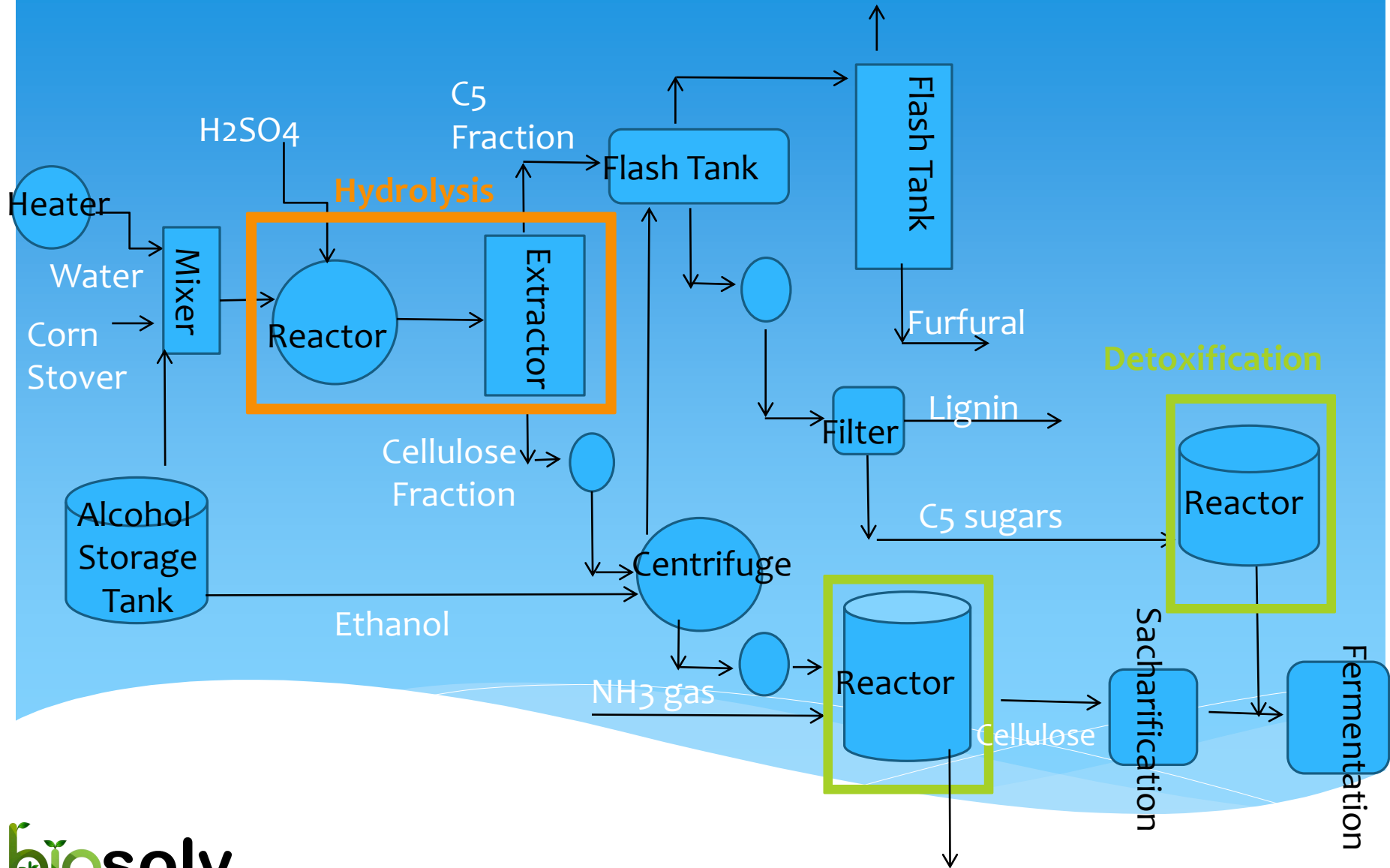
REV	DATE	BY
1	1/10/02	...
2	2/12/02	...
3	3/12/02	...


NREL National Renewable Energy Laboratory
 Biotechnology Center for Fuels and Chemicals

Overall Process
 Cellulosic Biomass to Ethanol
 10/2001-10/2002



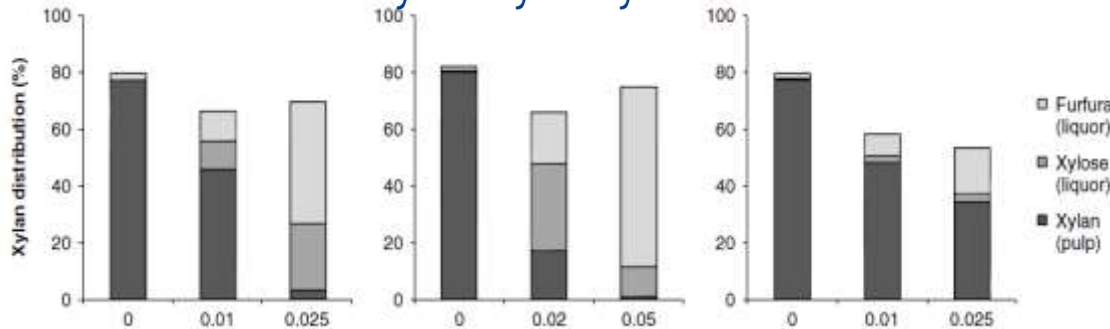
Process Overview



Optimization

Catalysts: H_2SO_4 , HCl, $MgCl_2$

Xylan hydrolysis

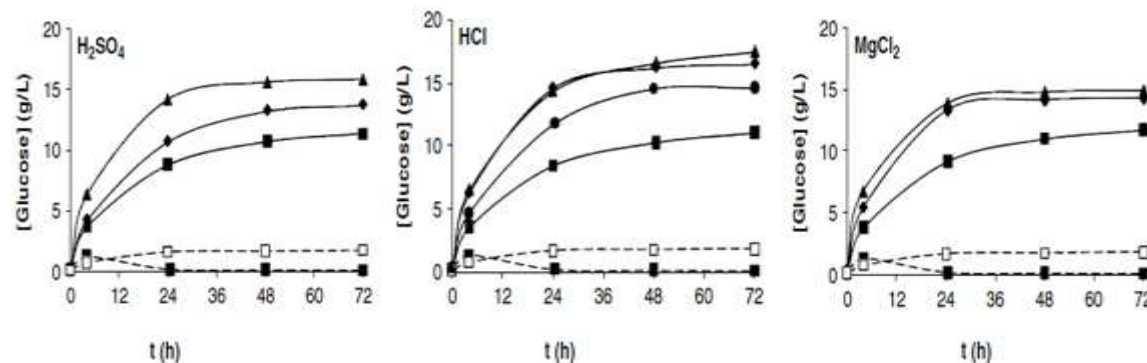


* H_2SO_4

* Weaker acid than HCl, but also less expensive and corrosive

* $MgCl_2$ gives a lower enzymatic glucose yield than the two acids.

Glucose yield



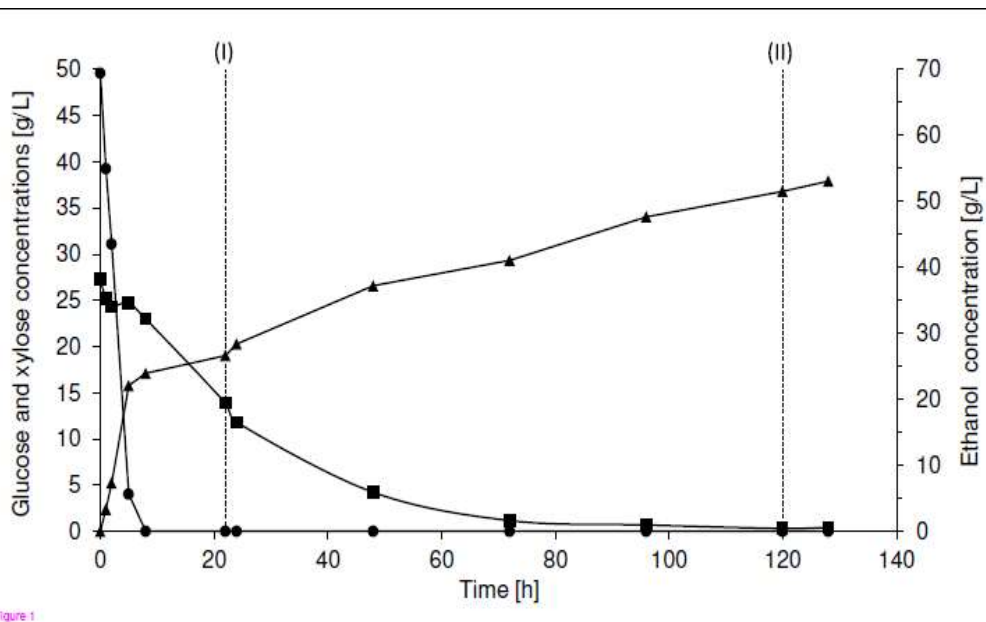
Optimization

Ethanol vs. Methanol

- * *Ethanol*
 - * Easy recovery
 - * Low cost

Separate vs. Co-fermentation

- * *Co-fermentation*
 - * Reduce vessel down time for cleaning – smaller plant is at an equal annual capacity
 - * Higher productivities than separate processes



Organosolv Flow Diagrams

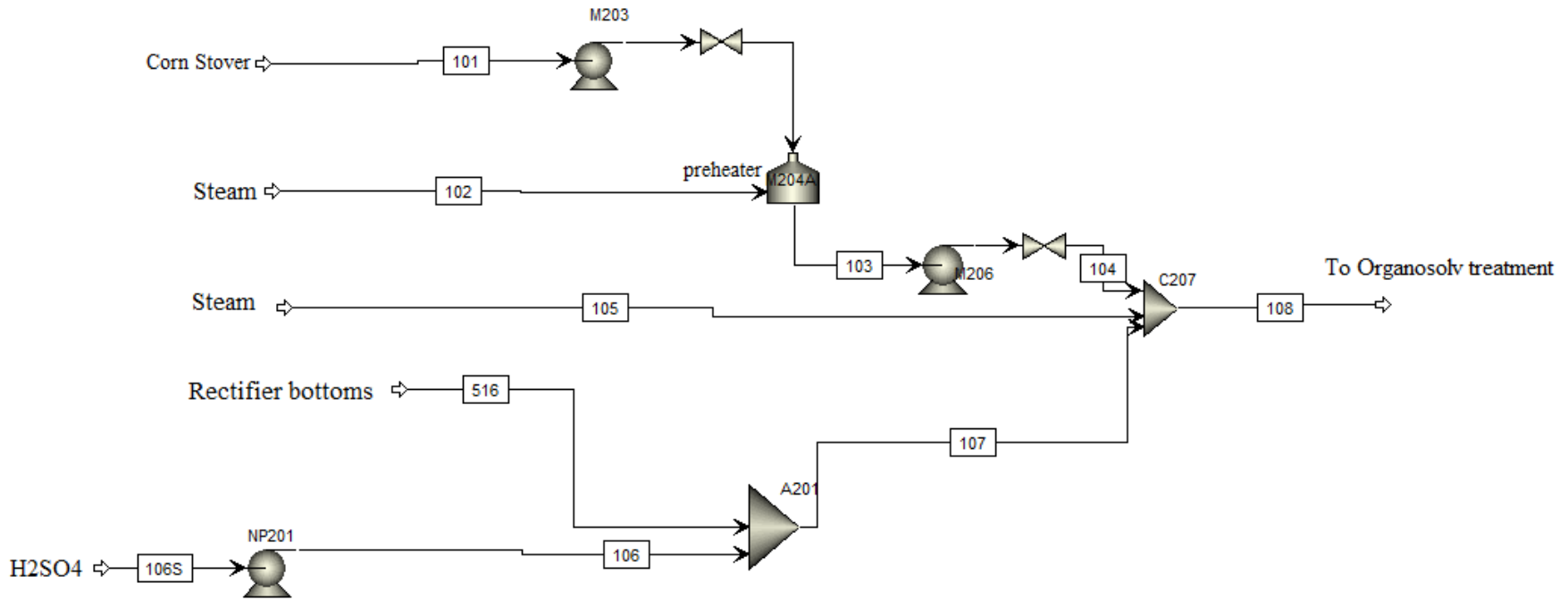
Pretreatment

Hydrolysis

C5 sugars

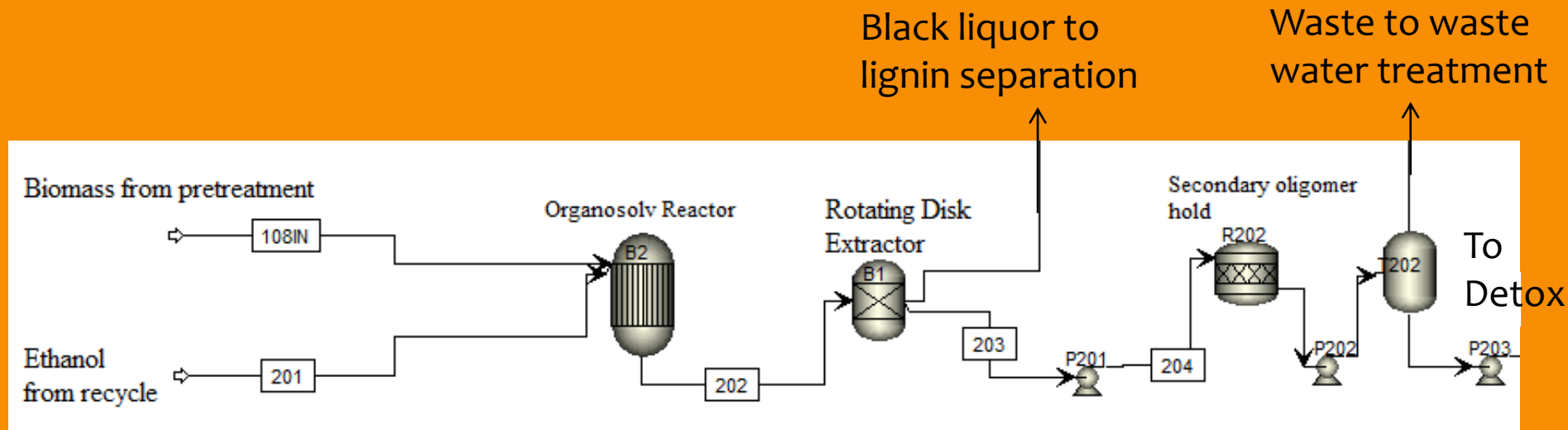
Fermentation
of C6 Sugars

Pretreatment



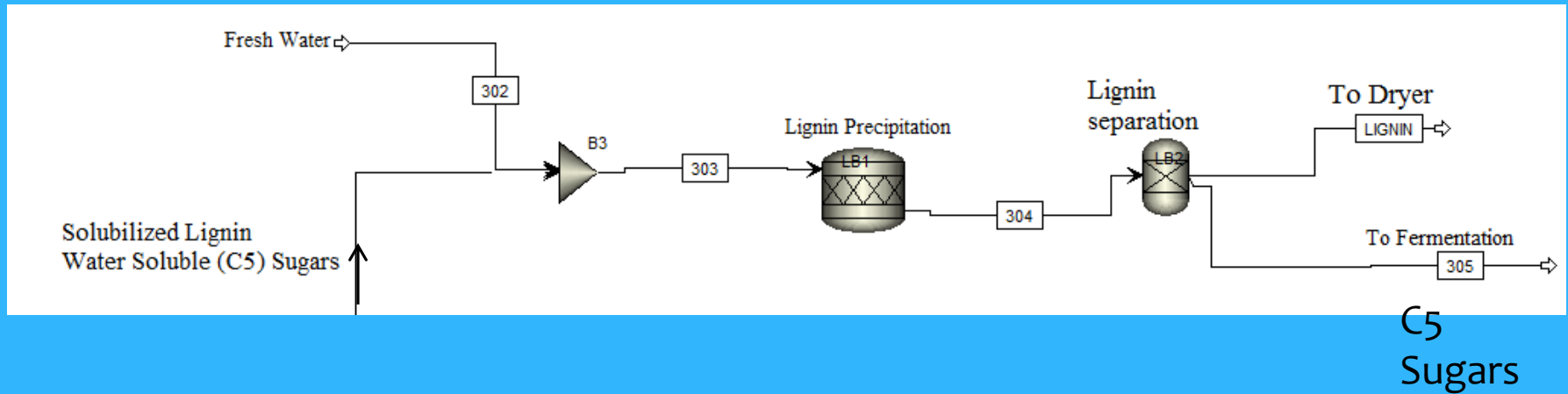
- Cornstover pulping
- Addition of steam and heat to break up lignin structure
- Initial addition of H₂SO₄ for hydrolysis

Hydrolysis



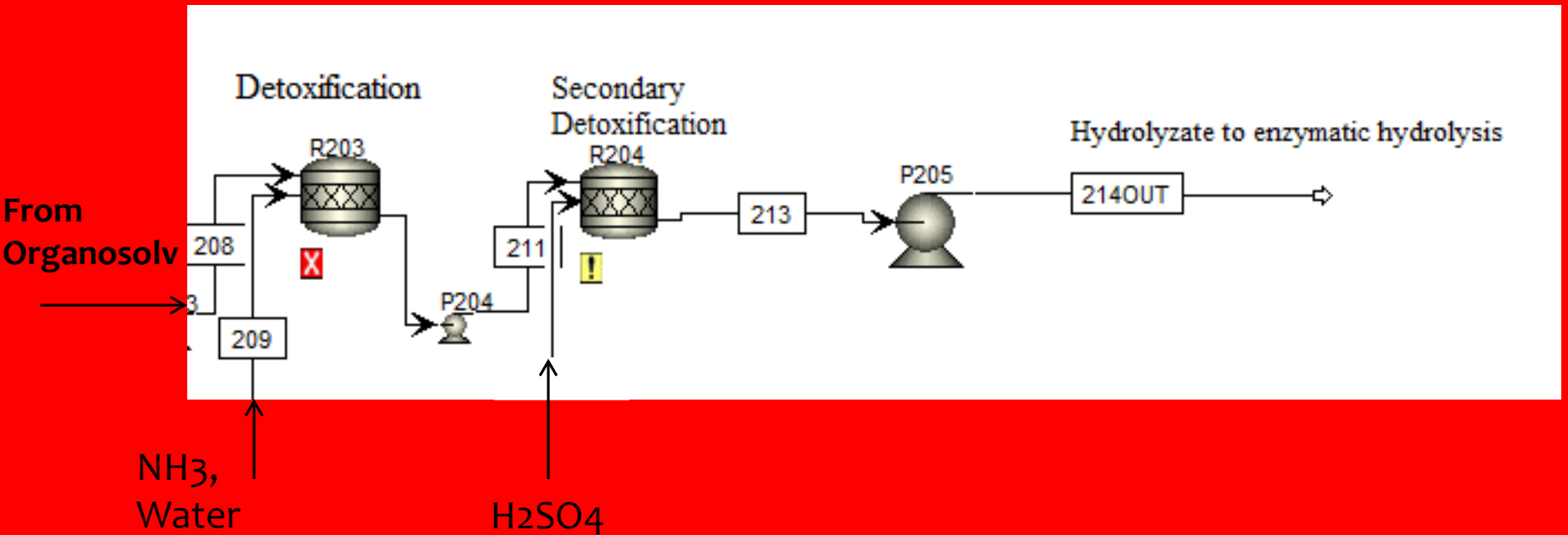
- Ethanol added for pulping, 50% (V/V)
- Pulped ~ 1 hour at 100°C, lignin solubilized
- Rotating Disk extractor removes liquor (C5 sugars, lignisol, and other by-products)
- Liquor sent to lignin separation unit, cellulose sent for further hydrolysis and saccharification and detox before fermentation

C5 Sugars



- Liquor from organosolv extractor washed with water, lignin precipitates
- Precipitate collected in filter and sent to dryer
- Filtered liquid with soluble sugars sent to fractional distillation for ethanol removal and then to fermentation

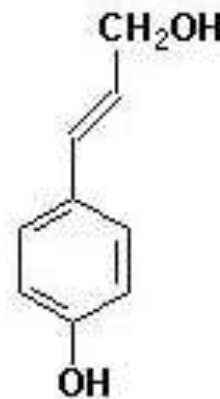
C6 Sugars



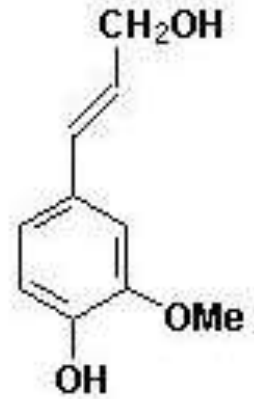
- Hydrolyzate from Organosolv detoxified with NH₃
- Secondary detoxification to bring hydrolyzate to ~pH 6.8-7.2

Byproducts: Lignin

- * Complex polymer with many forms and uses
- * Low grade: cattle feed additive, asphalt conditioner, binders in wood and other materials
- * High grade: specialty chemicals, pharmaceutical precursors, rubber additives
- * Growing global market and research area
- * \$0.20-3.50 per kg
- * Does not require very much extra equipment



p-hydroxyphenyl alcohol

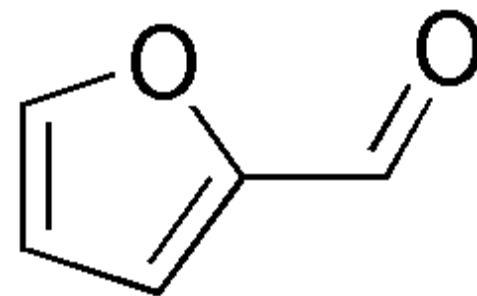


coniferyl alcohol

Precursors for lignin

Byproducts: Furfural

- * Organic compound used for chemical processes
- * Solvent or lubricator
- * Precursor starting material for other chemicals
- * Low demand; China produces most of world supply
- * \$1 per kg
- * Not enough produced to justify market risk or extra equipment



Business Opportunity

- * Demand for alternative energy; government requirements
- * More efficient process
- * Less pollutant

- * Midwest → Illinois
 - * Heavy farming
 - * Available feedstock
 - * Proximity to large cities



Economic Overview

- ❖ Based on the NREL study
 - ❖ Equipment Sizing
 - ❖ Operating Costs (Feed, Operating Conditions, etc.)
 - ❖ IRR, NPV, PBP
- ❖ Organosolv vs. NREL Pretreatment Analysis
- ❖ State & Federal Incentives
- ❖ Byproduct usability

Organosolv Economics

- ❖ Total installed cost of Organosolv pretreatment = \$21.5 million
- ❖ Total Capital Investment = \$368 million
- ❖ IRR (30 year base) = 15%
- ❖ Pay back period = 4.25 years



Organosolv Economic Issues

- * Not profitable as a standalone process
- * Highly dependent on incentives
- * Questionable byproduct market

OSHA & EPA

OSHA

- * Ventilation of CO₂
 - * Control the rate and order of chemical addition
 - * provide robust cooling
 - * segregate incompatible materials to prevent mixing
- * Large of amounts of water waste
 - * Bio electricchemical system for treatment
 - * Reduces green house gases
- * Burning furfural
 - * PEL: 5ppm 8 hr TWA

EPA

- * Positive affects of Ethanol on environment:
 - * Reduce carbon monoxide and nitrogen oxide outputs
 - * In surface water evaporates quickly
 - * Reduce green house gas emissions

Conclusion/Recommendations

- ❖ Organosolv is a better pretreatment option than current process
- ❖ Sellable lignin reduces boiler block and is profitable
- ❖ Lignin processing and stable market
- ❖ Continue project development

