

Development of a Low-Energy Consumption CO₂ Separation Method

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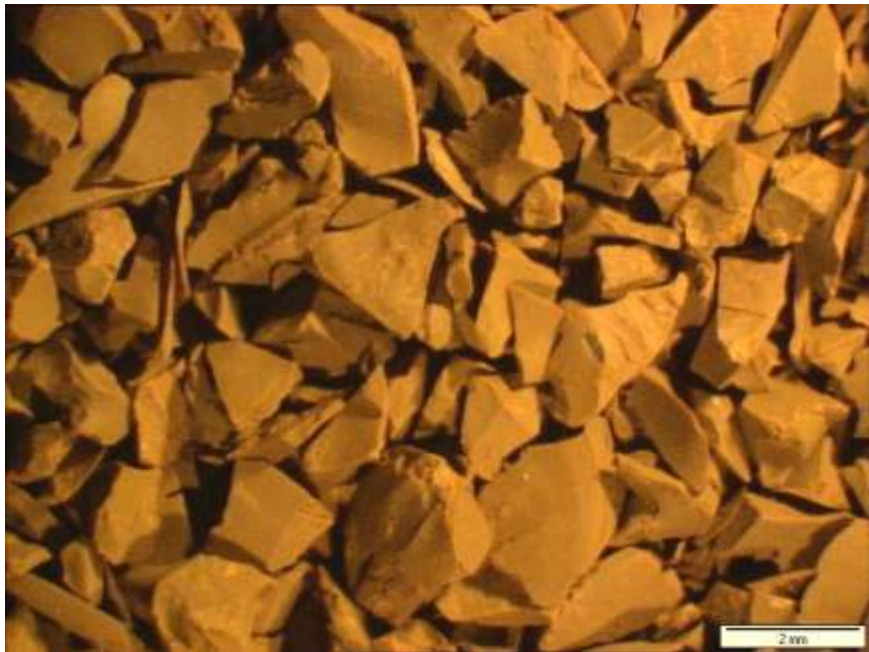
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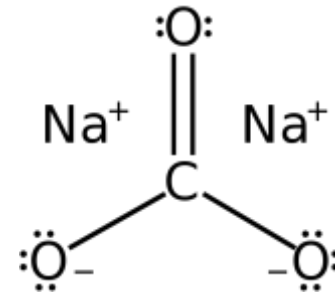
Background

- Many sorbents have been proposed for CO₂ separation.
- As a solid sorbent; alkali metal based sorbents have a great potential for inexpensive CO₂ removal.
- Na₂CO₃/FeOOH was synthesized and compared to K₂CO₃ properties.

Background



Iron Oxide (FeOOH)



Sodium Carbonate (Na₂CO₃, i.e. soda ash)

Background

	Na₂CO₃	K₂CO₃
Molecular Weight (g/mol)	105.9	138.2
ΔH (kcal/mol)	-270.3 exothermic	-274.9 exothermic
ΔG (cal/mol*K)	99.2	57.26
ΔS (cal/mol*K)	33.2	37.32
Cost/lb	\$0.27	\$1.07

Current Challenges

- Many CO₂ removal methods are already employed in industry.
- Current methods are expensive to replace.
- NETL developing a promising new aqueous ammonia system.

Technical Merits

- Use of nanoporous support material for an increased CO₂ sorption capacity.
- Use of catalytic function of the same support material could improve desorption kinetics of CO₂ during regeneration.

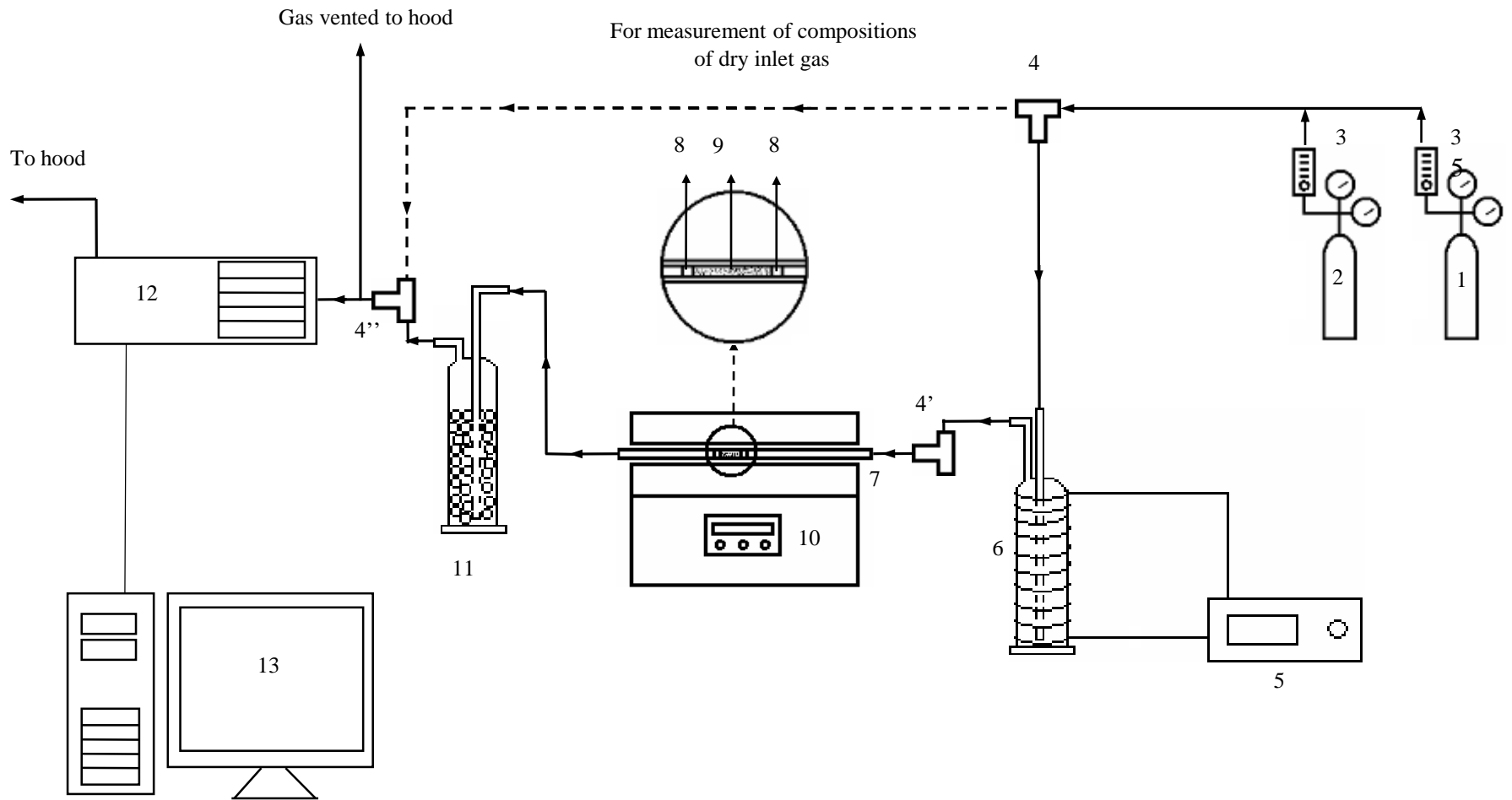
Preparation

- Nanoporous FeOOH was prepared using well known sol-gel and hydrolysis methods.
- 99.5% Anhydrous Na₂CO₃ was purchased from VWR.
- Wet impregnation was used to prepare the solid sorbent Na₂CO₃/FeOOH.

Methods

1. X g of Na_2CO_3 was dissolved in 50mL of deionized water (where X varies from 2.5 -10 g of Na_2CO_3).
2. 10 g of nanoporous FeOOH was then added to the solution and was dissolved over a 24 hr period at 400 rpm.
3. After 24 hrs, the deionized water is evaporated off at 56 C on a rotovap leaving the prepared sorbent behind.

Experimental Set-up



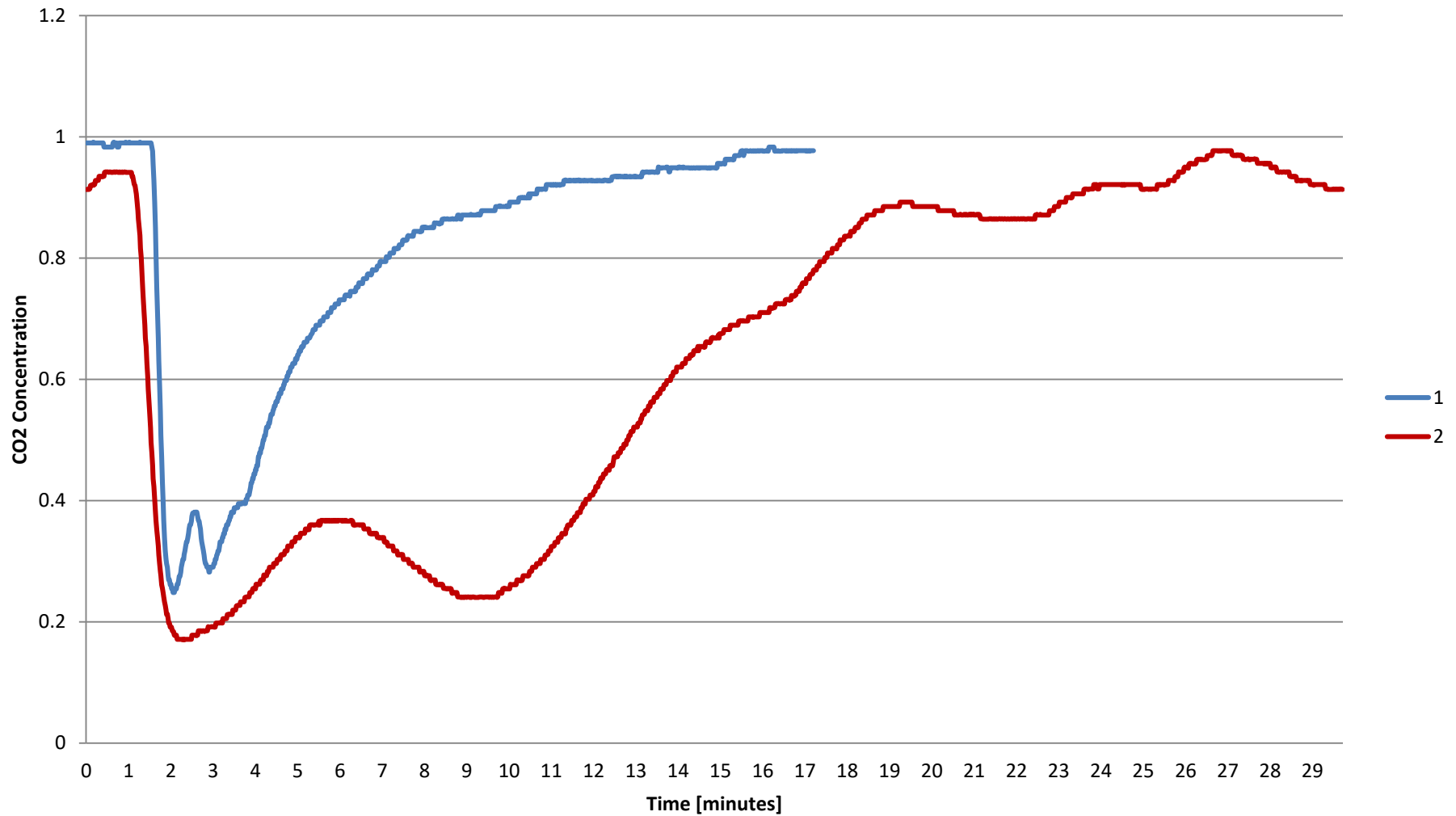
Synthesized Sorbents

Support Material FeOOH	Sorbent Na ₂ CO ₃
grams	grams
10	2.5
10	5
10	7.5
10	10

- Experiments conducted utilizing a 1% CO₂ gas stream.

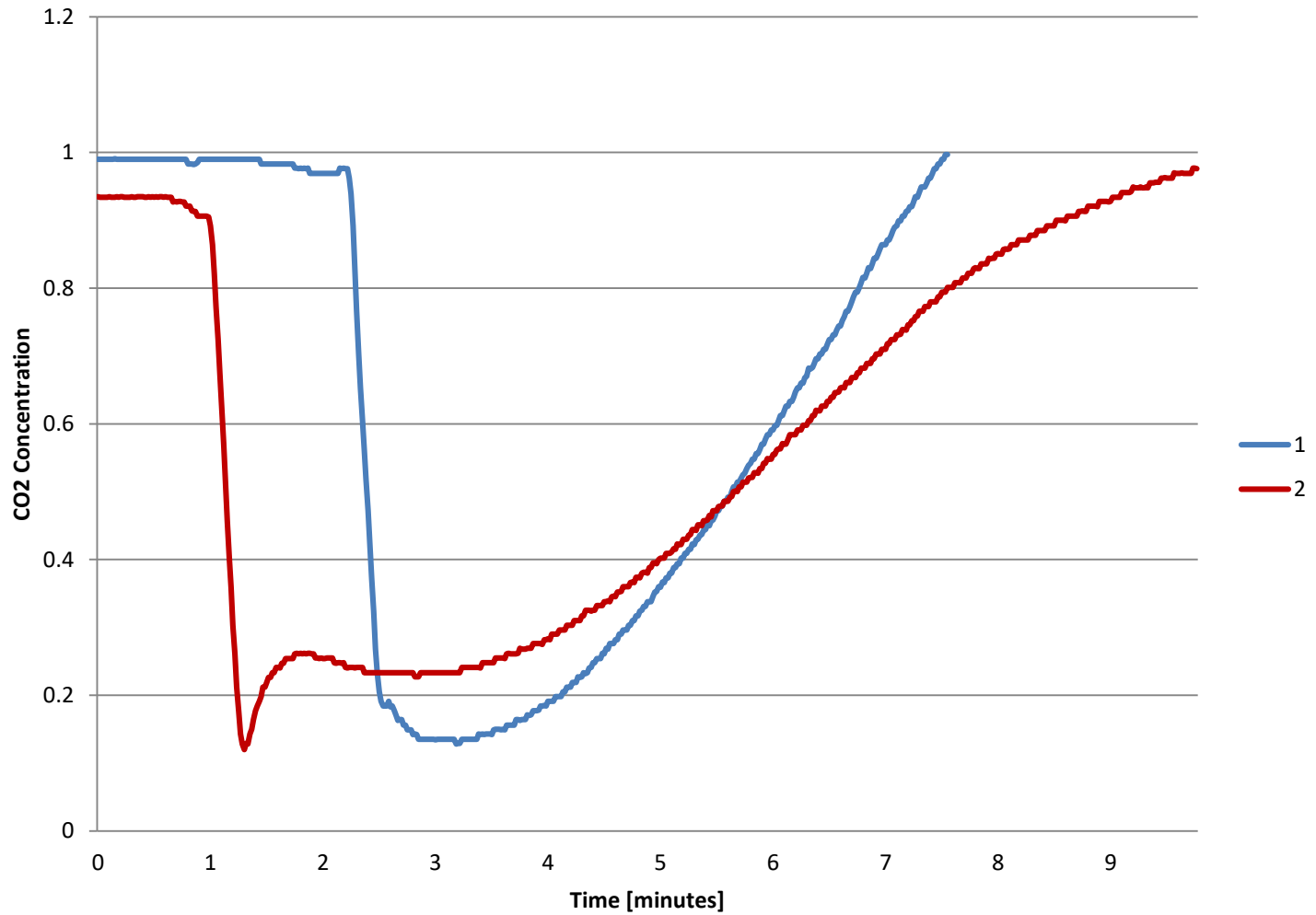
Results

2.5Na₂CO₃/10FeOOH



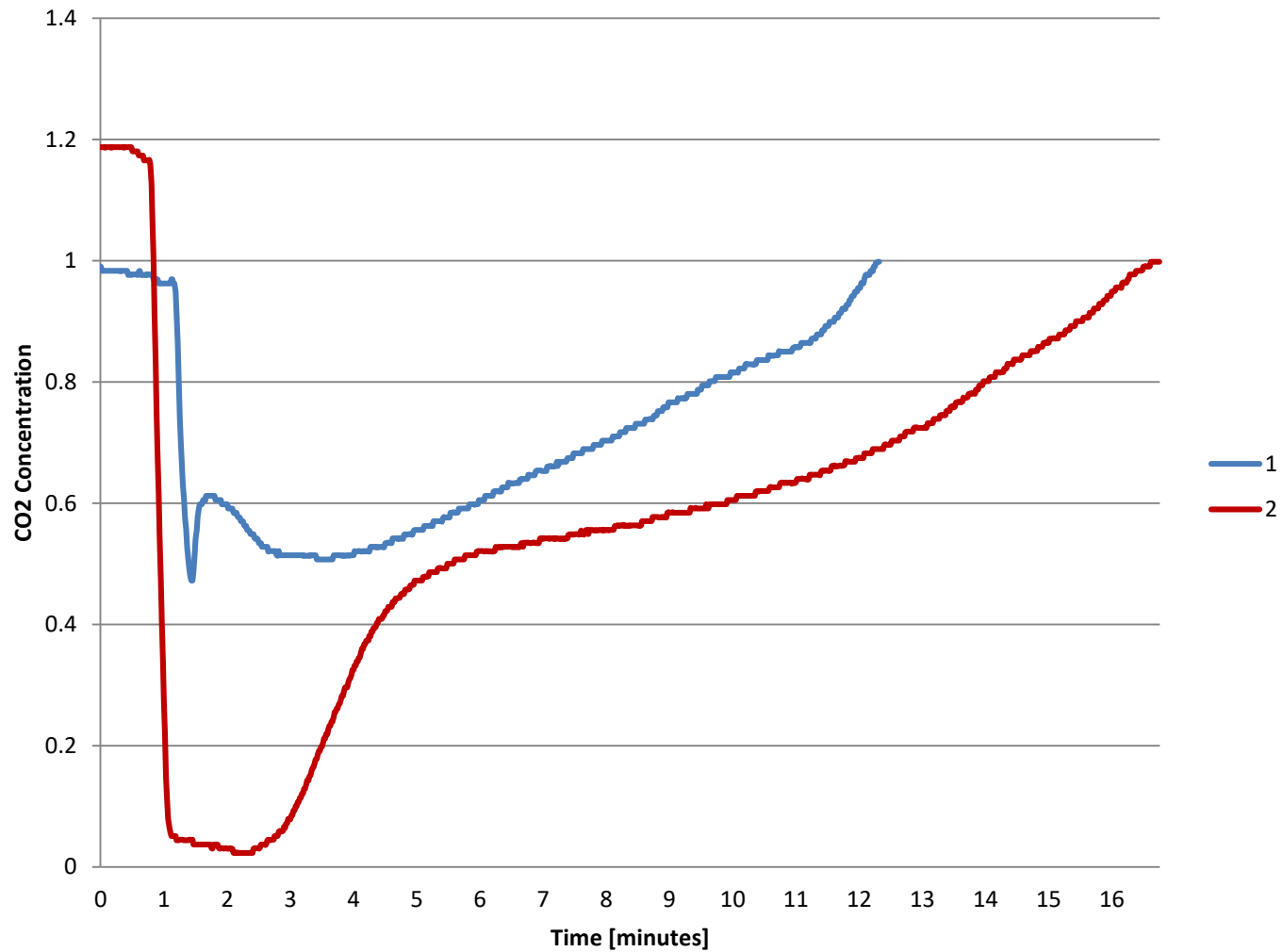
Results

5Na₂CO₃/10FeOOH



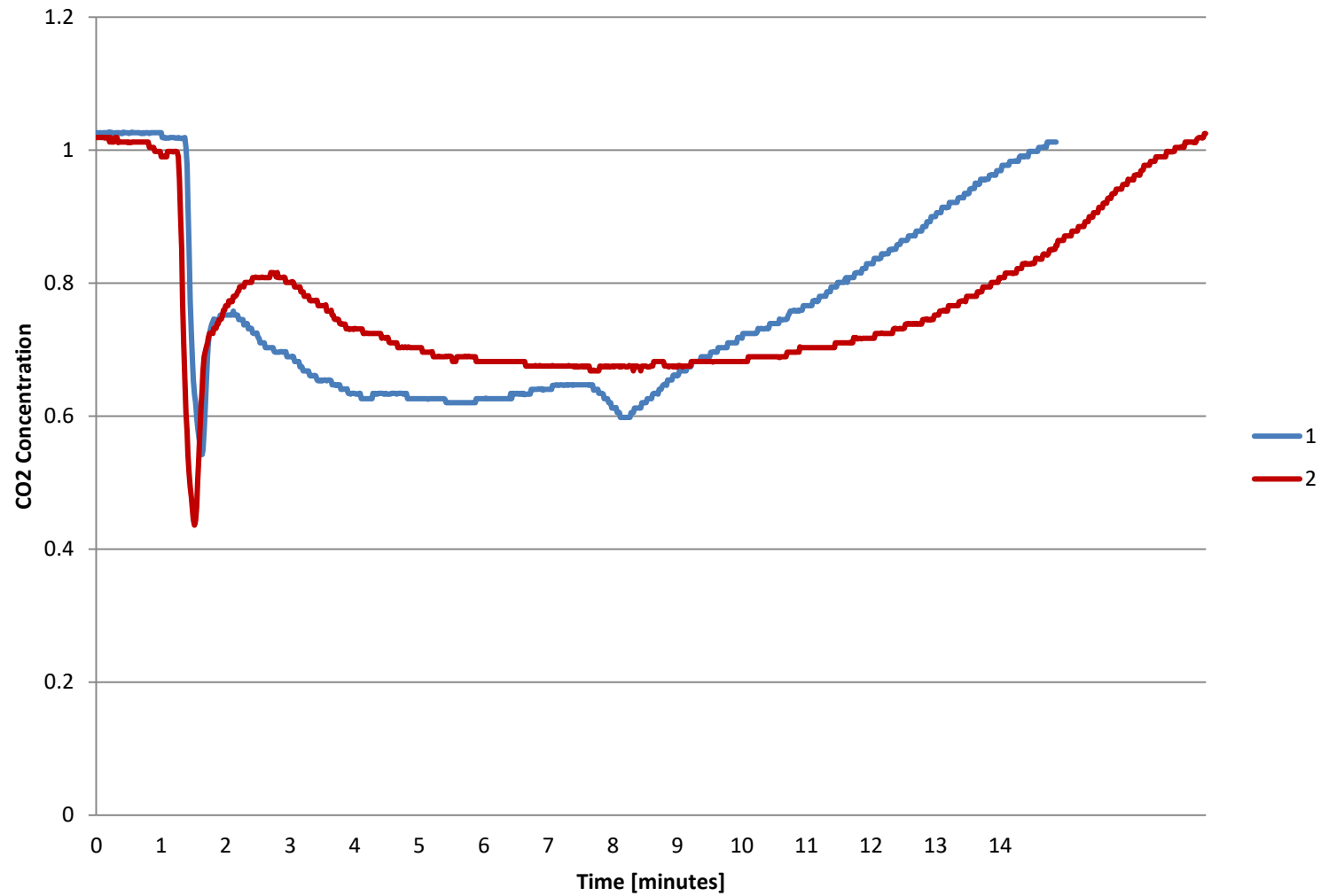
Results

10FeOOH/7.5Na₂CO₃



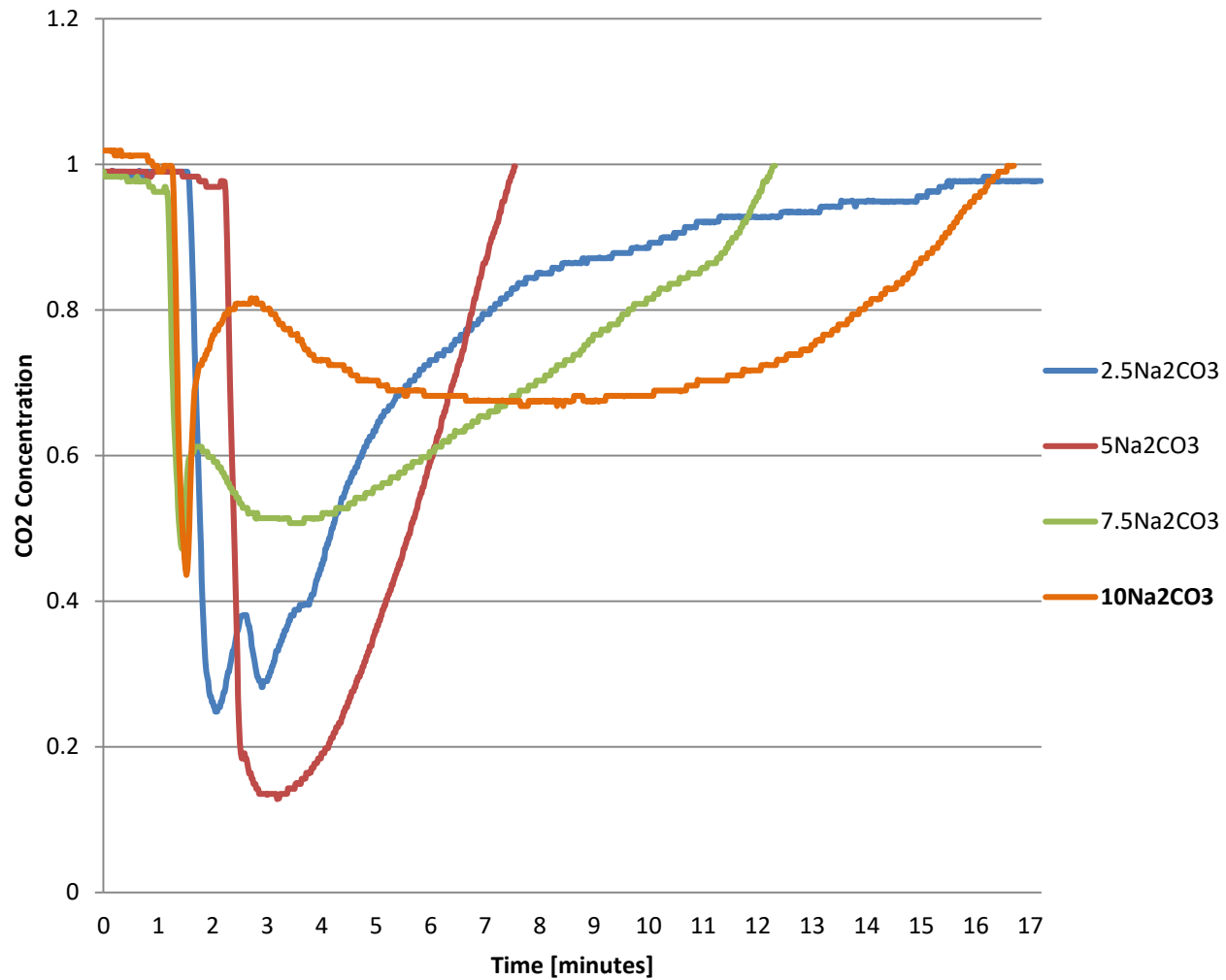
Results

10Na₂CO₃/10FeOOH



Results

Comparison



Summary

- Based on the above graphs. I believe that the best sorbent choice would be $10\text{Na}_2\text{CO}_3/10\text{FeOOH}$.
- This is because it has the largest surface area of Na_2CO_3 available for CO_2 adsorption on the supporting material.
- The adsorption curve also shows that it has the most holding capacity for CO_2 .

Summary

- Based on the previously seen properties of Sodium Carbonate and Potassium Carbonate I believe that it would be about 3x more economical to use Sodium Carbonate over Potassium Carbonate for CO₂ removal.

Summary

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Limitations

- Only $\text{Na}_2\text{CO}_3/\text{FeOOH}$ was synthesized in the lab.
- Due to time limitations a limited number of runs were conducted.
- Limited availability of equipment; not able to use an XRD to verify structure of sorbents.

Further Research

- Further research should be done to determine the exact kinetics of this sorption.
- Mass transfer calculations need to be done to determine the exact amount of CO₂ adsorbed onto the chosen alkali sorbent.
- K₂CO₃/FeOOH needs to be synthesized to in the same lab to compare these sorbents side by side.

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Questions?

References

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